

# BVT

# TECHspec

Wyatt Engineering Badger Venturi Tube  
Primary Flow Element Design



**Pressure Vessel, Nonimpact Design**

Based on the classical venturi design, nonimpact venturi meters are those that sense only axial components of the line fluid's velocity profile; nonaxial vectors are considered insignificant in standard piping. The resulting flow meter has a discharge coefficient ( $C_D$ ) that approaches unity, is not a function of fluid velocity and beta ratio ( $d/D$ ), and is constant above a given threshold pipe Reynolds number. In general, designs that utilize this flow metering mechanism are less sensitive to upstream pipe fittings than those designs that employ other types of pressure sensation.

The BVT nonimpact design conforms to all those characteristics that make venturi meters the preferred flow meter when accuracy, reliability, and low permanent pressure loss are required. The value and performance of the nonimpact BVT  $C_D$  indicates an extremely efficient metering shape and independence of line velocity; only pipe Reynolds number ( $R_D$ ) is a concern. If the pipe Reynolds number is greater than 75 000, the substantiated uncertainty of the BVT design is better than  $\pm 0.50\%$ ; for  $R_D < 75\ 000$ ,  $C_D$  is known and repeatable.



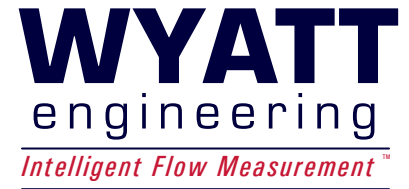
**Insert-Type, Impact Design**

Insert-type, impact venturi meters sense a nonaxial velocity component in their high pressure sensation. As a result, the meter discharge coefficient is dependent on beta ratio; however,  $C_D$  is not a function of line velocity and is still constant above a given threshold pipe Reynolds number.

The BVT impact flow meter is a cost-effective alternative to the nonimpact pressure vessel design. While slightly more sensitive to upstream piping than the nonimpact design, these insert-type venturi meters provide the same accuracy, reliability, and low pressure loss as that of the nonimpact design.

Though a function of beta ratio, the impact BVT  $C_D$  provides the same efficient metering shape and independence from line velocity as the nonimpact BVT: If  $R_D \geq 75\ 000$ , then the uncertainty is better than  $\pm 0.50\%$ ; for  $R_D < 75\ 000$ ,  $C_D$  is predictable and repeatable. Contact Wyatt Engineering for further information.

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# Installation Effects

The differential pressure produced by the BVT design is an indication of the difference in the kinetic energy of the line fluid between the high and low pressure tap cross sections. Due to differing velocity profiles, a given flow rate can possess different kinetic energies, and thereby introduce errors in the indicated flow rate. This is the essence of the study of installation effects and installed accuracy.

These curves summarize the results of flow tests on nonimpact BVT flow meters. The “nonimpact” term reflects the condition that neither the high nor the low pressure tap senses nonaxial velocity components. This refers to meters commonly (but erroneously) labeled “static tap” design. The most common Wyatt Engineering model numbers appropriate for these data are: BVT, BVT-B, BVT-F, and BVT -U.

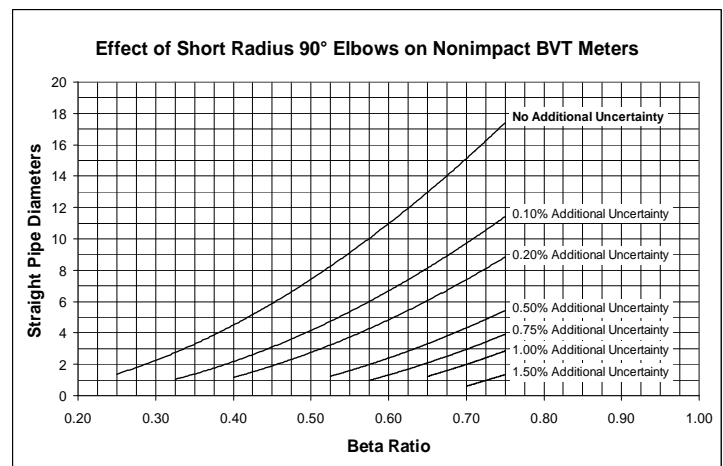
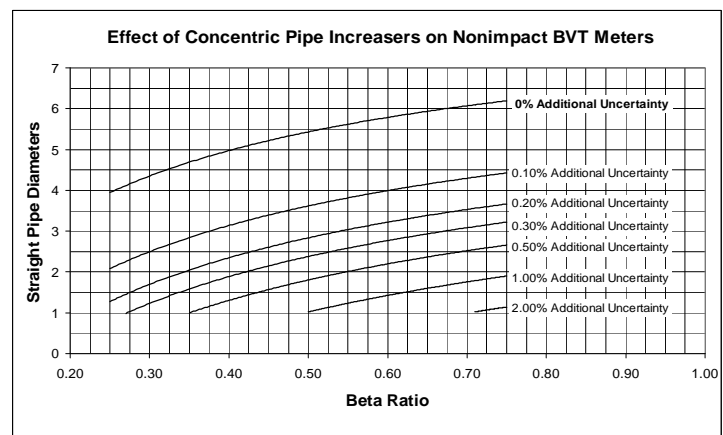
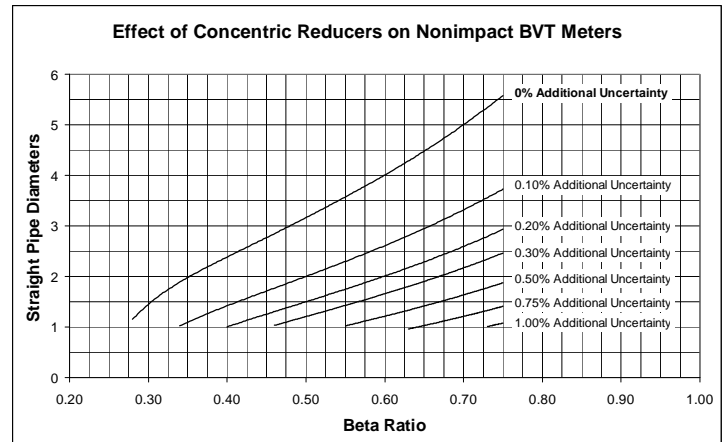
One concept made clear immediately by these test results is meter sensitivity to an upstream disturbance decreases with decreasing beta ratio (d/D). Put more simply: **The smaller the beta ratio, the smaller the effect of upstream piping.** Note that a similar relationship exists for orifice meters, flow nozzles, and nozzle venturi meters. Stated differently, if  $E_I$  is the installation error function, then

$$\lim_{\beta \rightarrow 0} E_I = 0$$

Given this relationship by itself, logically, one should design differential producers with beta ratios approaching zero! In general, the great compromise is: The smaller the beta ratio, the higher the permanent pressure loss. While the desire is to minimize both the specific headloss and installed uncertainty, increased permanent pressure loss is sometimes the cost of improved installed accuracy.

Flow patterns that change the behavior of the discharge coefficient can be caused by pipe fittings, Reynolds number, and/or pipe surface/diameter irregularities. From flow testing, we have learned the following: The smaller the meter beta ratio, the smaller is the effect of pipe fittings; and irregular flow patterns that are nonrotational, that is, those caused by reducers, single elbows, etc., are self-attenuating, while irregular flow patterns that are rotational, for example, those caused by two elbows direct-coupled in perpendicular planes, are relatively stable and users should consider flow straighteners in such cases.

With respect to downstream piping requirements, pipe fittings, valves, etc. may be direct-coupled to the outlet of the BVT venturi meter without affecting the accuracy. Note that some meters’ recovery sections are truncated, so direct-coupling a butterfly valve may, in some instances, cause the valve disk to interfere with the meter outlet and full valve disk movement may not be possible. Let us know if this configuration is required and the meter outlet will be modified accordingly. It should be noted also that the pressure loss of the direct- or close-coupled valve or pipe fitting will be somewhat higher than is calculated assuming a blunt velocity profile. If this is a concern, please contact Wyatt Engineering for further assistance.





# Uncertainty Substantiation

Sample	Inlet Dia.	Throat Dia.	Beta Ratio	Calibrated C <sub>D</sub>	Predicted C <sub>D</sub>	Deviation in C <sub>D</sub>	Test Facility
1	1.050	0.314	0.2990	0.9923	0.9918	0.050%	Badger
2	1.935	1.119	0.5783	0.9960	0.9946	0.141%	Alden
3	3.052	1.840	0.6029	0.9927	0.9897	0.303%	Alden
4	3.062	1.840	0.6009	0.9895	0.9898	-0.030%	Alden
5	3.139	2.318	0.7385	0.9961	0.9957	0.040%	Alden
6	3.823	2.492	0.6518	0.9728	0.9755	-0.277%	Alden
7	3.826	1.634	0.4271	0.9956	0.9910	0.464%	CEESI
8	4.026	1.710	0.4247	0.9926	0.9910	0.161%	Badger
9	4.028	1.709	0.4243	0.9919	0.9910	0.091%	Badger
10	4.971	2.657	0.5345	0.9839	0.9802	0.377%	Alden
11	4.971	2.657	0.5345	0.9807	0.9802	0.051%	Alden
12	6.040	3.715	0.6151	0.9610	0.9622	-0.126%	Alden
13	6.057	3.610	0.5960	0.9600	0.9585	0.156%	Alden
14	6.065	3.640	0.6002	0.9970	0.9984	-0.140%	Badger
15	6.068	3.915	0.6452	0.9875	0.9894	-0.192%	Badger
16	6.067	3.914	0.6451	0.9894	0.9870	0.243%	Badger
17	7.282	3.813	0.5236	0.9883	0.9903	-0.202%	Alden
18	7.980	3.333	0.4177	0.9905	0.9910	-0.050%	Badger
19	7.981	4.804	0.6019	0.9941	0.9948	-0.070%	Badger
20	8.005	3.604	0.4502	0.9853	0.9839	0.140%	Alden
21	8.010	5.552	0.6931	0.9425	0.9397	0.298%	Alden
22	8.028	4.720	0.5879	0.9776	0.9800	-0.245%	Alden
23	8.125	3.393	0.4176	0.9887	0.9910	-0.232%	Badger
24	8.127	3.393	0.4175	0.9923	0.9910	0.131%	Badger
25	9.119	3.953	0.4335	0.9850	0.9851	-0.014%	Alden
26	11.965	6.668	0.5573	0.9718	0.9726	-0.083%	Alden
27	12.000	7.245	0.6038	0.9951	0.9948	0.030%	Badger
28	12.000	7.248	0.6040	0.9984	0.9948	0.362%	Badger
29	12.059	7.066	0.5860	0.9719	0.9680	0.404%	Alden
30	12.300	6.923	0.5628	0.9679	0.9718	-0.399%	Alden
31	13.424	6.596	0.4914	0.9814	0.9804	0.101%	Alden
32	15.250	11.435	0.7498	0.9846	0.9850	-0.041%	Alden
33	15.380	8.443	0.5490	0.9688	0.9738	-0.512%	Alden
34	15.550	8.272	0.5320	0.9752	0.9760	-0.081%	Alden
35	17.250	9.410	0.5455	0.9779	0.9743	0.374%	Alden
36	17.762	9.114	0.5131	0.9764	0.9782	-0.182%	Alden
37	19.190	12.931	0.6738	0.9426	0.9435	-0.095%	Alden
38	19.236	10.455	0.5435	0.9712	0.9745	-0.341%	Alden
39	19.480	13.740	0.7053	0.9277	0.9288	-0.118%	Alden
40	19.500	9.509	0.4876	0.9814	0.9808	0.065%	Alden
41	19.508	9.358	0.4797	0.9787	0.9815	-0.284%	Alden
42	23.250	12.505	0.5378	0.9743	0.9753	-0.098%	Alden
43	23.250	12.505	0.5378	0.9751	0.9753	-0.016%	Alden
44	23.352	11.637	0.4983	0.9809	0.9797	0.120%	Alden
45	29.250	17.937	0.6132	0.9651	0.9626	0.258%	Alden
46	29.484	18.850	0.6393	0.9857	0.9895	-0.384%	Alden
47	35.243	12.008	0.3407	0.9851	0.9903	-0.523%	Alden
48	35.250	13.928	0.3951	0.9900	0.9876	0.248%	Alden
49	35.250	13.928	0.3951	0.9877	0.9876	0.015%	Alden
50	35.500	19.337	0.5447	0.9867	0.9901	-0.343%	Alden

Test data covers the pipe Reynolds number range of 40 000 to 4 850 000.

Uncertainty is a calculated value, not an opinion. The method outlined above is the correct approach; anything else is sales talk.

## The Uncertainty of a BVT without Flow Calibration

The vast majority of BVT flow meters are provided without flow calibration. This is due to our ability to substantiate the uncertainty of the BVT to within  $\pm 0.50\%$  of indicated flow rate for pipe Reynolds numbers greater than 75 000.

For the BVT meter design, there is a “true” discharge coefficient ( $C_D$ ). The true  $C_D$  can be estimated only through repeated observations, but those observations (flow calibrations) will have uncertainties associated with them. The observed  $C_D$ , therefore, equals the true  $C_D$  plus an attendant uncertainty band. The error on the estimated discharge coefficient,  $C_D$ , is reduced to zero as the number of flow calibrations approaches infinity.

Since there are not an infinite number of flow calibrations, we must consider the contribution of the finite sample size to the combined uncertainty. Note that this allowance, formerly referred to as precision, is often neglected in many uncertainty calculations provided by the ill-informed or inexperienced. It is necessary, however, because it accounts for the finite size of the sample.

For the calibrations shown, the standard uncertainty of the data is  $\pm 0.24\%$  and consideration for the small sample is  $\pm 0.07\%$ . Together, this provides a combined uncertainty of  $\pm 0.25\%$ , which, in turn, results in an expanded uncertainty of  $\pm 0.49\%$  at a 95% confidence interval.

**BVT Uncertainty  
without Flow Calibration**

**$\pm 0.49\%$**

